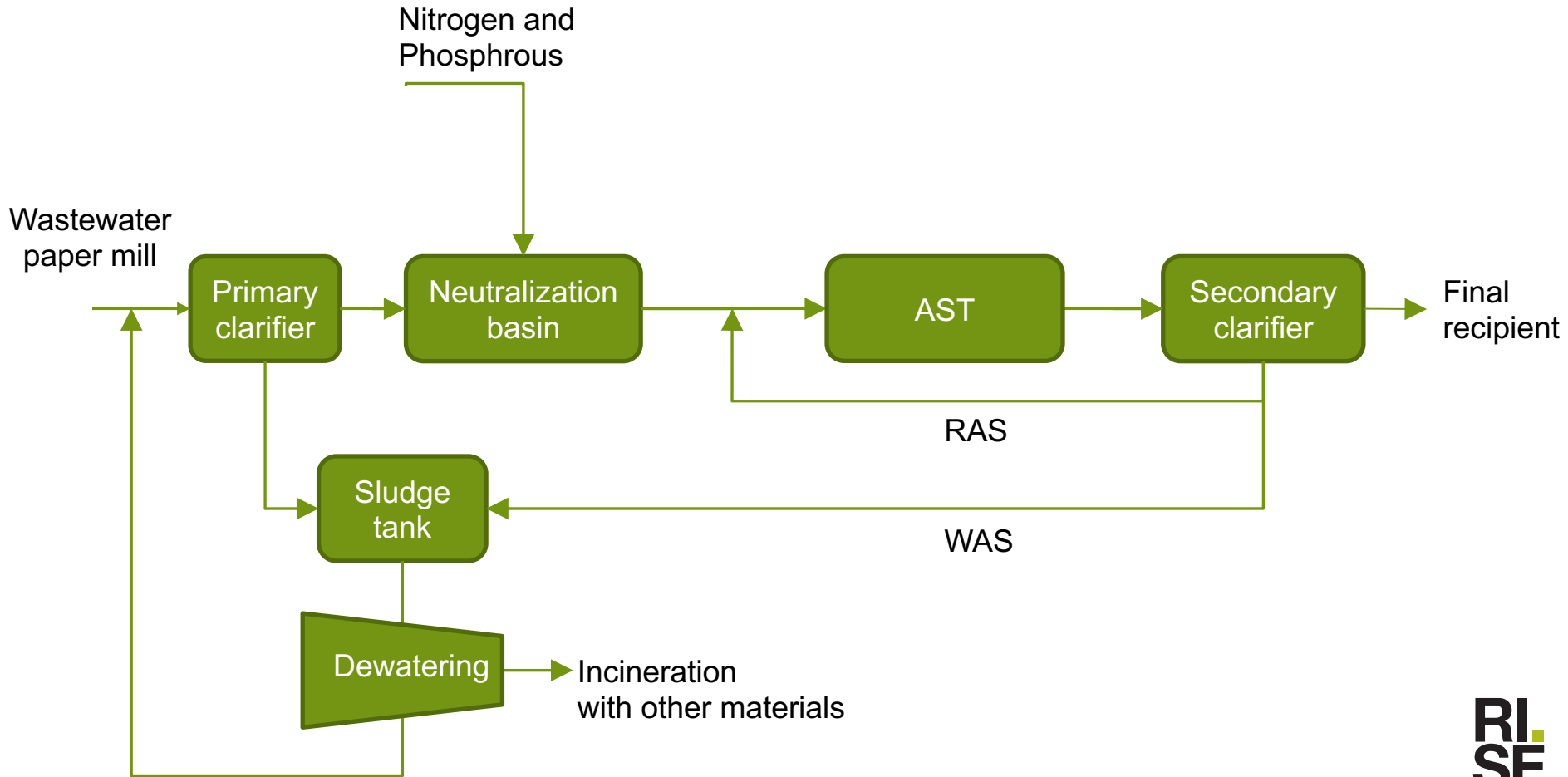
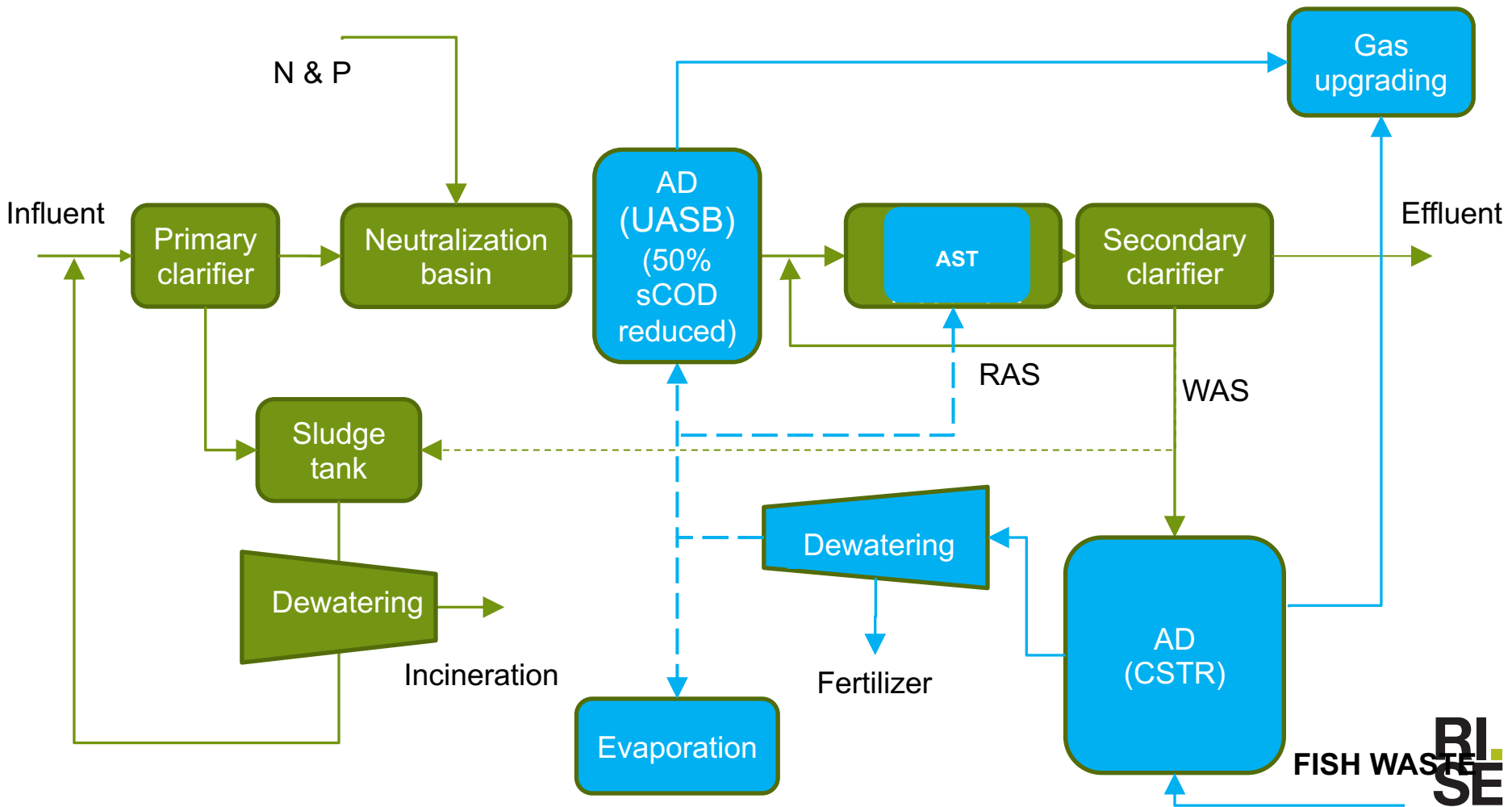


Modelling and Simulation to Assess Industrial Symbiosis

Magnus Arnell,
RISE Research Institutes of Sweden







Process Modelling

Introduction

- The purpose of models is to reflect the real world system in order to understand them
- Model development must take a stance in the problem formulation for which the model will be used
 - The best model is the simplest one possible to address problem
- Models are useful but never correct


**The main problem in
our field is to keep
the main problem
the main problem**

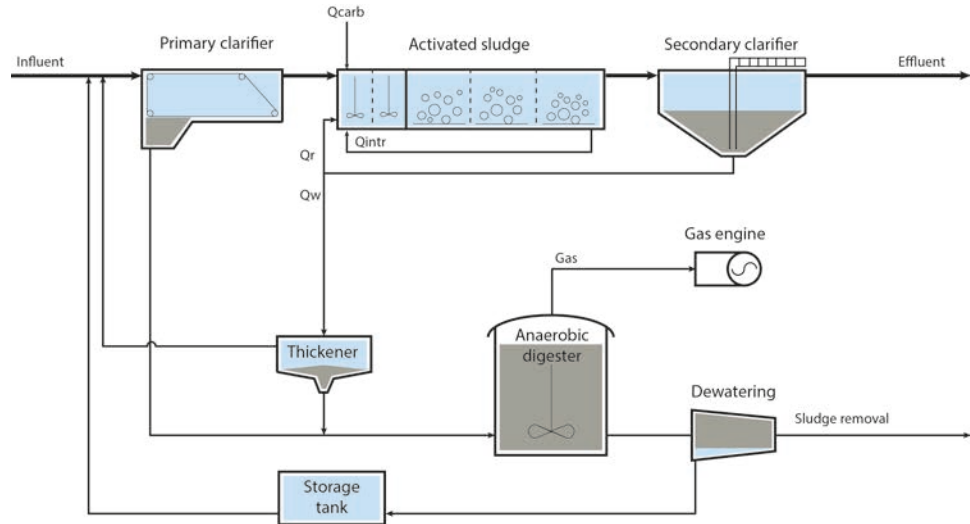
– George Ekama

Modelling goals

- WWTP modelling for developing process understanding
- Modelling for WWTP design
- Modelling for WWTP optimisation
- Modelling for WWTP control
- WWTP modelling for teaching/learning
- Digital Twins

WWT Process Model

- Hydraulics
 - Biological processes
 - Chemical Processes
- 
- Sub models
 - Activated sludge
 - Anaerobic digestion
 - Settling
 - Etc.
 - Mathematical equations implemented in a computational software for simulations



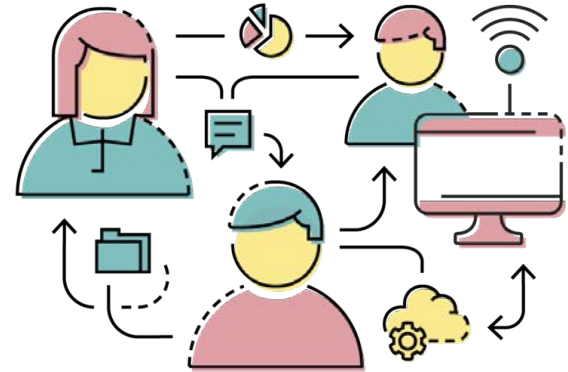
Case Study – Skogn

Aim and purpose of modelling

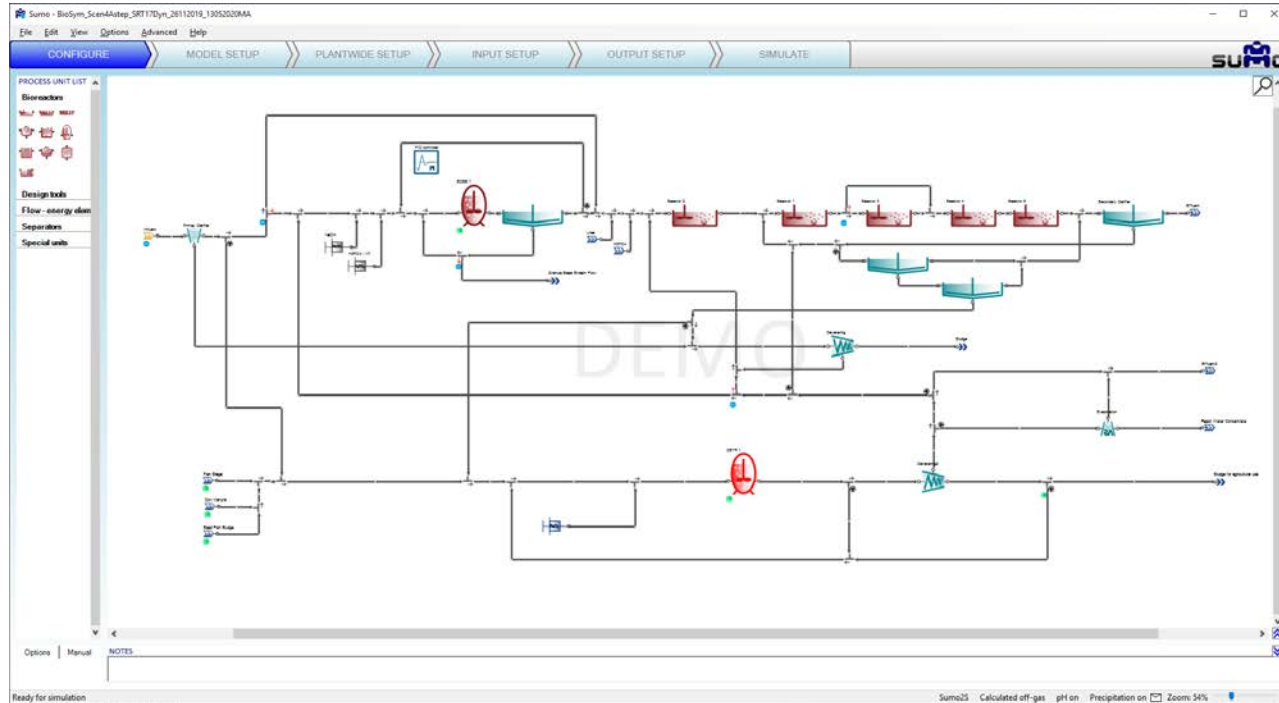
- Evaluate plant-wide impact of industrial symbiosis concept
 - Impact on effluent water quality
 - Evaluate plant operational strategies, incl. disturbances
 - Optimize nutrient additions
 - Optimize co-substrate mix
 - Communication purposes

Model developments

- Physico-chemical modelling
- Sulfur conversion and reactions
- Granular anaerobic process
- (Methane oxidation)

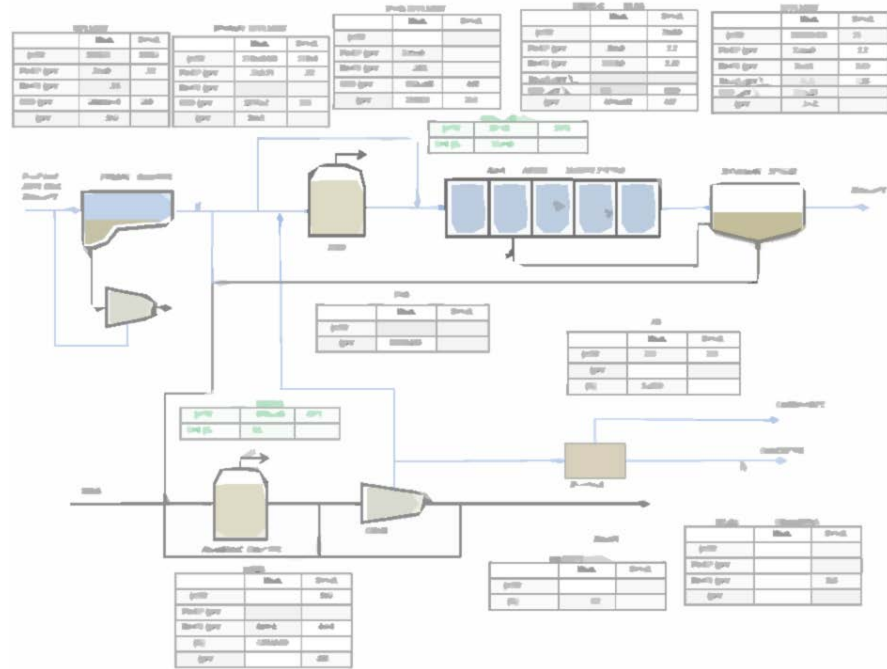


SUMO modelling software



Model calibration and validation

- Following Good Modelling Practice
- Thorough data collection campaigns
- Influent characterization
- Calibration of model parameters until criteria
- Validation on separate data set
- Static and dynamic



Results

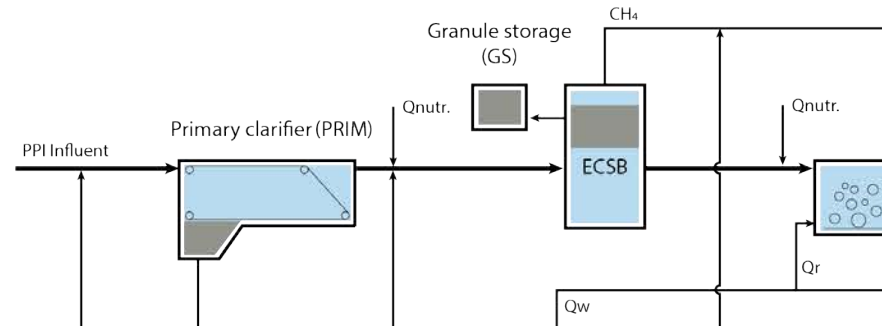
COD load and characteristics

COD fractionation – 7 variables

- Volatile fatty acids (VFA)
- Readily biodegradable substrate (non-VFA)
- Slowly biodegradable substrate
- Soluble unbiodegradable organics
- Particulate unbiodegradable organics
- etc

Transformation of COD

- Mechanical separation
- Microbial growth on substrate (varying conditions)
- Decay and hydrolysis



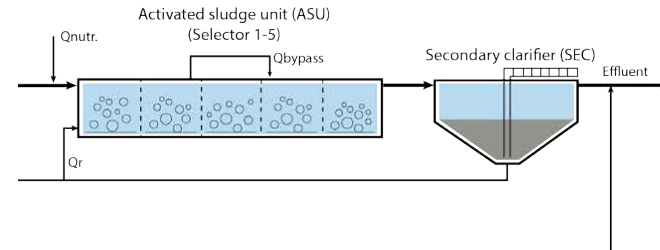
Activated sludge operation

Transformation of COD

- Aeration requirement is reduced
- Operational strategy analysed, e.g. by-passing of Selector 3

Predicting

- Higher COD-content of WAS
- Lower fraction of COD in WAS is unbiodegradable
- → Biogas potential higher

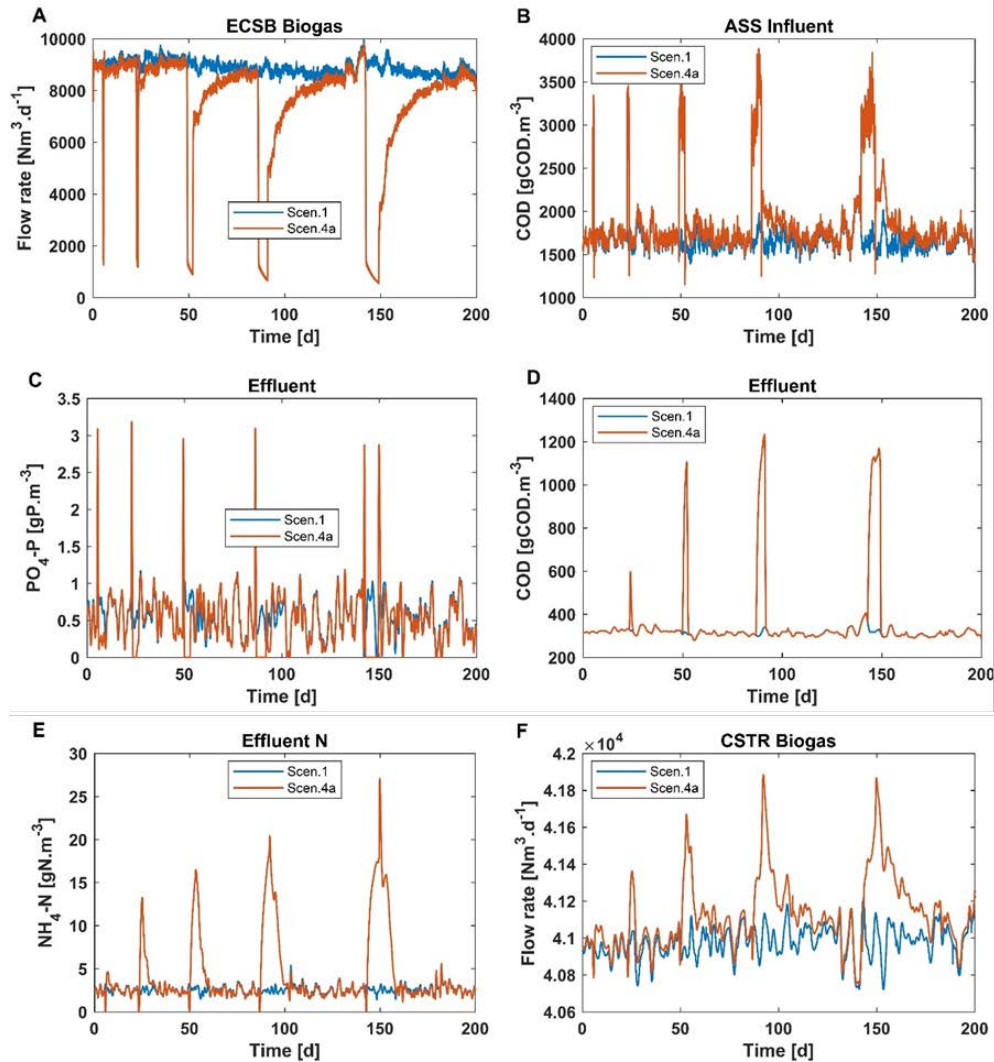


Nutrient optimization

Scenario	Nutrient dosing				Effluent quality		
	N reject water (kgN.d ⁻¹)	P reject water (kgP.d ⁻¹)	H3PO4 ECSB (kgP.d ⁻¹)	H3PO4 ASS (kgP.d ⁻¹)	N (kgN.d ⁻¹)	P (kgP.d ⁻¹)	COD (kgCOD.d ⁻¹)
Nutrient optimization	-17 %	-18 %	-100 %	-100 %	Improved	Improved	Similar
Nutrient optimization – reduced SRT	-8 %	-2 %	-100 %	-62 %	Similar	Improved	Similar

ECSB bypass

- Disturbance case – short term bypass of primary effluent over ECSB to activated sludge
- Time for bypass: 0,5, 1, 3, 5, 7 days.
- 0,5 and 1 days – limited impact.
- 3, 5, 7 days – prolonged impact.



Conclusions technical



- Predict the characteristics of the COD to ASS as a result of adding an ECSB
- Assessment of operational strategy for ASS with reduced load
 - lower SRT and bypass of Selector 3 is possible
 - the lower load also means a reduced need of aeration in the ASS
- Predict how the sludge age in the ASS affect the biodegradable organics in the WAS
 - the slowly biodegradable COD is roughly doubled.
 - this indicate an improved biomethane potential of the WAS.
- Nutrient dosing optimizations identified and savings estimated
- Assessment of the effect of ECSB-bypass on the ASS at different time length
- Sulphur conversion processes shown and fate of S predicted

Conclusions general



- Model developed in commercial platform with success
- Important output variables are predicted – averages and trends in simulated scenarios
- Simulations provided valuable process insights during commissioning of full-scale process
- Simulation results are valuable for communication with plant operations, contractors etc.
- Model adaptable to other plants through re-characterization and re-calibration

Where to go from here..

- Literature review
- Project report
- Project website



Magnus Arnell

Magnus.arnell@ri.se

010-516 63 33