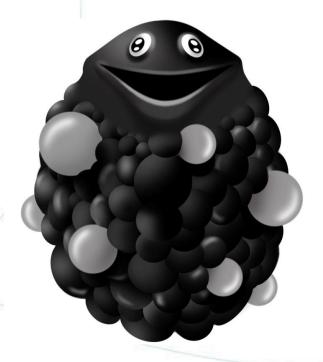
### Major reactor development for anaerobic treatment in the pulp and paper industry

Norrköping 7 November 2018

**Leo Habets** 

<u>l.habets@paques.nl</u> +31653827804





- 1 History of sludge bed reactor development
- 2 Introduction of a new type reactor

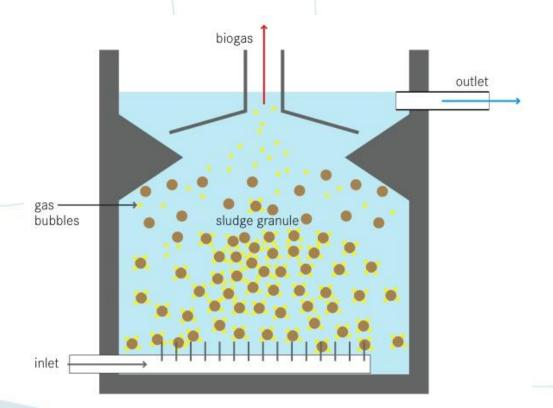
- 3 Number of sludge bed reactors in P&P
- 4 conclusions



#### Invented in the 70-ties in Wageningen (group Gatze Lettinga)

# **Upflow Anaerobic Sludge Blanket**

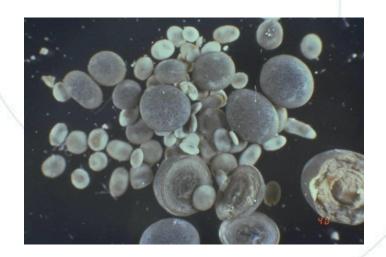
**UASB** 





Trials started in 1981 at Roermond Papier (NL)

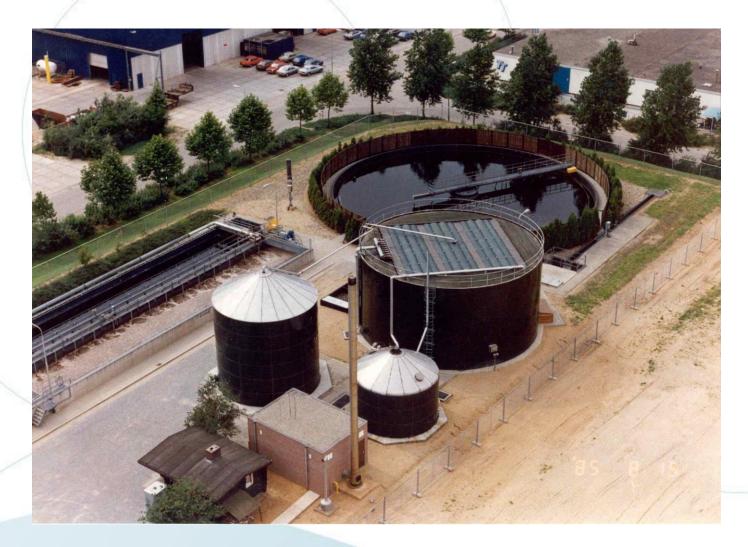
confirmed granulation







### Initial square UASB settler design at Smurfit Kappa Roermond Papier in 1983



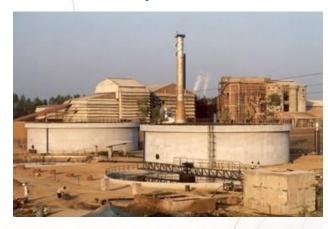


#### Circular UASB settler design in 1994 and later

#### **Industriewater Eerbeek 1985**



Satia Paper India 1994







#### Move to modular settler design as of 1987

#### For retrofit



#### and new









### Modular UASB plant design at Paper Mill in Aschaffenburg (1990)



and at SK Zülpich papier closed circuit (1995)



### Invented at Paques in the 80-ties

(by Sjoerd vellinga of Paques BV)

# Internal Circulation

#### **IC** reactor

**Applied since 1996** 





#### **Need for robust design and good process control**







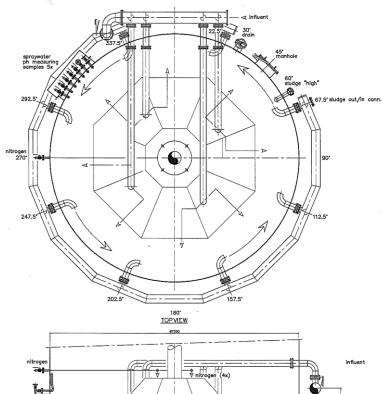


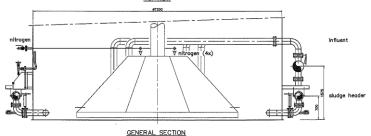


#### **Inlet distribution by** "mixing chamber" and sludge extraction by ring line











#### Inlet header and sludge extraction ring line





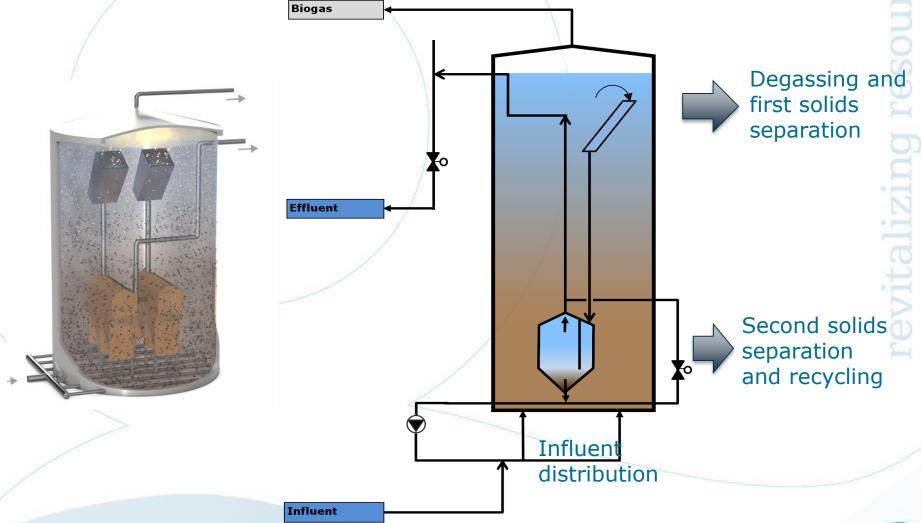
- 1 History of sludge bed reactor development
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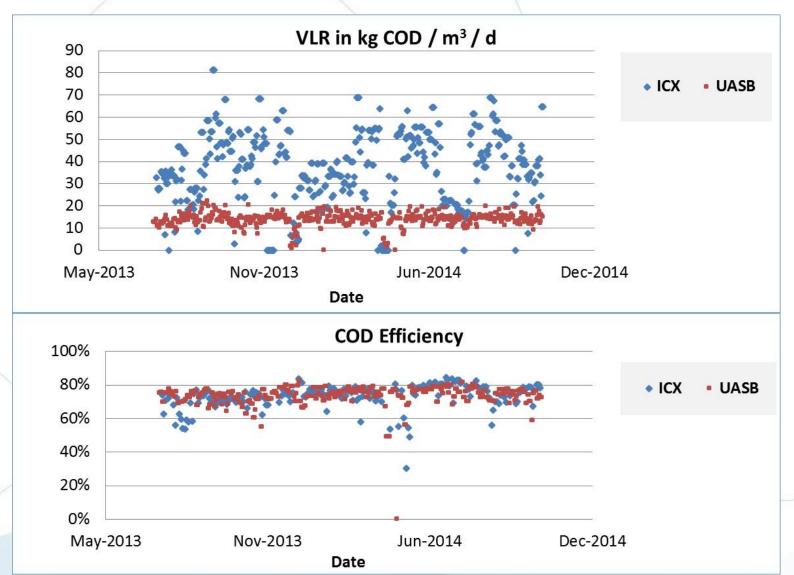
#### **BIOPAQ ICX reactor schematically**

invented by Rienk Prins of Paques BV





# Results of the 1.5 year 100 m3 demo ICX in parallel to UASB on paper mill effluent

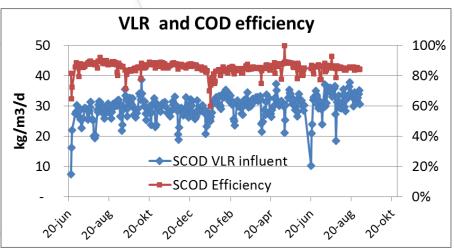


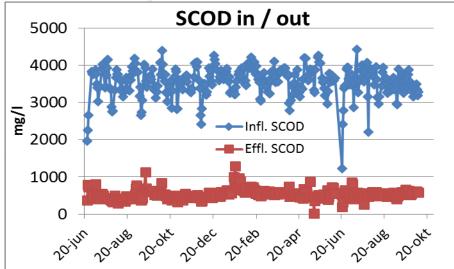


### First full scale ICX replaces fluidized bed at Allard Emballage in France



Ø4m x 16m (200m<sup>3</sup>) 6 t COD/d





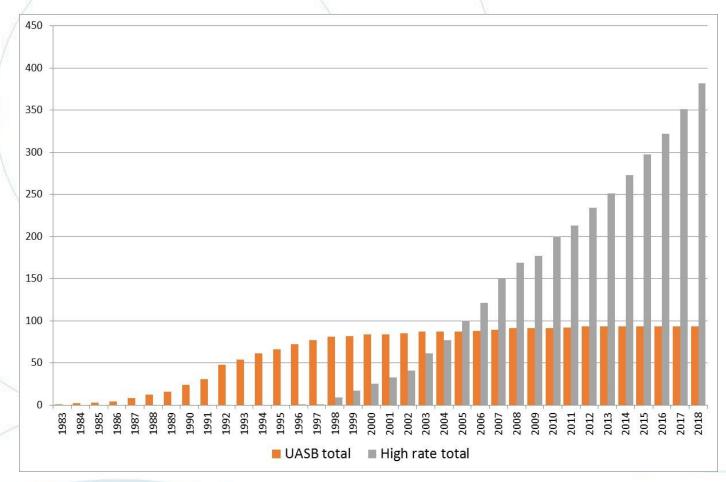


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## Cumulative number of UASB and high rate (EGSB + IC + 'IC' +ICX) reactors in P&P





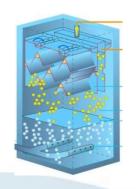
#### Overview of Biopaq anaerobic plants in P&P (2016)





#### Reactor design parameter comparison

	UASB	EGSB	IC	ICX
Height (m)	5 - 6	14 - 19	20 - 28	14 - 17
Upflow (m/h)	0.8 - 1.0	3 - 6	8 - 12	4 - 8
Typical VLR kgCOD/m3.d	10	15	20 - 25	20 - 30











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#### **Conclusions**

- Continuous move towards smaller footprint and lower cost reactors
- More efficient use of volume and flexibility in tank sizing
- Robust design and corrosion free internals
- Closed reactors to prevent odor; for safety and no effluent overflow weirs to be cleaned
- Trend to more modular design



